



Hydrogen Production by Nuclear Power

Practical Pathways for Gradual Realization

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Need for Hydrogen in Non-Electricity Energy Sectors

Global energy-related CO2 emission by sector



 CO_2 emission reduction through the use of hydrogen in industrial and transportation sectors

Energy storage and feedstock synthetic fuels

Fuel cells for heavy duty vehicles and building heating

Steel production by hydrogen reduction and other uses

Industry

Transport

Hydrogen production

Nuclear electricity and heat

Hydrogen Production Methods

Water Electrolysis			Chemical Water Splitting	5. Steam Methane
1. Alkaline Electrolysis (AE)	2. Proton Exchange Membrane (PEM)	3. Solid Oxide Electrolysis (SOE)	4. Sulfur-Iodine Cycle (S-I)	Reforming (SMR)
Operating Temperature 60~90 ℃	50~90 ℃	High Temperature Steam Over 700 ℃	850 °C	Over 700 °C
Features ✓ Proven method ✓ Cost effective ✓ Cheap catalyst × Low pressure × Low flexibility × Low gas purity × Corrosive electrolyte	 ✓ High pressure ✓ High current density ✓ High gas purity ✓ Flexibility × Expensive catalyst × High cost 	 ✓ Heat energy use ✓ High current density ✓ High gas purity ✓ High efficiency ✓ Cheap catalyst × Low pressure × First-mover-disadvantage 	 ✓ Heat energy use ✓ High efficiency ✓ Closed system ✓ Continuous production × Corrosive environment × Expensive material × Not yet verified 	 ✓ Proven technology × Highest CO₂ emission
AEC e' e' e' e' e' e' e' e' e' e'		SOEC SOEC Solution Ha	$\begin{array}{c} T^{AC} \\ 1000 \\ 000 \\ H_{3}SO_{4}(\mathbf{g}) \rightarrow H_{2}O(\mathbf{g}) + SO_{3}(\mathbf{g}) + 1/2O_{3}(\mathbf{g}) \\ H_{3}SO_{4}(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) + 1/2O_{3}(\mathbf{g}) \\ H_{3}SO_{4}(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) + 1/2O_{3}(\mathbf{g}) \\ H_{3}SO_{4}(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) + H_{3}O(\mathbf{g}) \\ H_{3}SO_{4}(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \\ H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \\ H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \\ H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \\ H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \\ H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \\ H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \rightarrow H_{3}O(\mathbf{g}) \\ H_{3}O(\mathbf{g}) \rightarrow H_{3}O$	$(1) \qquad \qquad$

Source: Korea Institute Energy Research (2022).

Source: T. Proll and A. Lynngfelt (2022)Source: BASF (2019).

Source: Q. Wang (2022).

Limitation of Renewables Due to Low Capacity Factors



Intermittent and variable electricity input causes instability in electrolyzer
 Low capacity factor leads to higher electricity cost and electrolyzer cost

* Internal calculation by KAERI based on two assumed values of CAPEX and electricity price.

Advantage of High Temperature Steam Electrolysis with Nuclear Power





SOEC:	Solid Oxide Electrolysis
LWR:	Light Water Reactor
HTGR:	High Temperature Gas Cooled Reactor

Status of High Temperature Steam Electrolysis with Nuclear Power

USA



- 100 kW Bloom energy HTSE system is being operated at INL
- Xcel Energy will install a 100+ kW HTSE system at an NPP in the Minneapolis/St. Paul region
- APS is evaluating the integration of a HTSE system at its Palo Verde Nuclear Generating Station

*Arizona Public Services





The Prairie Island nuclear power plant (Photo: Xcel Energy)



Bloom prototype 100 kW HTE system at INL Source: INL, 2022

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High Temperature Gas Reactors



Technical characteristics

Heat supply capability (550~ 900°C)				
Safety features (TRISO coated fuel)				
Technical maturity				
Nuclear non-proliferation and security				

Potential benefits

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- Low carbon energy source
- > High-temperature heat supply

Reliability and flexibility

Better Possibilities with High Temperature Gas Reactors

Steam Methane Reforming with Carbon Capture and Sequestration

CH₄+H₂O→CO+3H₂ (206 kJ/mol) CO+H₂O→CO₂+H₂O



High Temperature Steam Electrolysis with SOEC



https://www.toshiba-energy.com/en/hydrogen/rd/

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Challenges in Sulfur-Iodine Chemical Cycle even with the Availability of High Temperature Heat



Critical point regarding both energy and efficiency

- HI_x Section (a mixture of iodine and iodides)
 - A large thermal burden (decrease of the global efficiency) due to
 - Azeotropic composition in the HI/H_2O system (at about 57% w/w)

 - Excess of water and iodine from Bunsen reaction
- Electrodialysis (ED) was proposed to concentrate HI aqueous solutions.
- The ED system is still having a **high electricity consumption**.

Practical Pathways for Nuclear Hydrogen Production

- Alkaline Electrolysis with Operating Nuclear Reactors
- High Temperature Steam Electrolysis with Operating and Newly Built Reactors
- Steam Methane Reforming with High Temperature Gas Reactors
- HTSE with HTGR
- Chemical Splitting with HTGR





Thank You

